

# Numerical research on conjugate heat transfer for batteries at CMT

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**Xandra Margot<sup>1</sup>, Kundan Kumar, Cem Karaca<sup>2</sup>**

**<sup>1</sup>CMT-Clean Mobility & Thermofluids**  
*Universitat Politècnica de València. Spain*

**<sup>2</sup>Departamento de Ingeniería**  
*Università degli Studi di Perugia. Italy*

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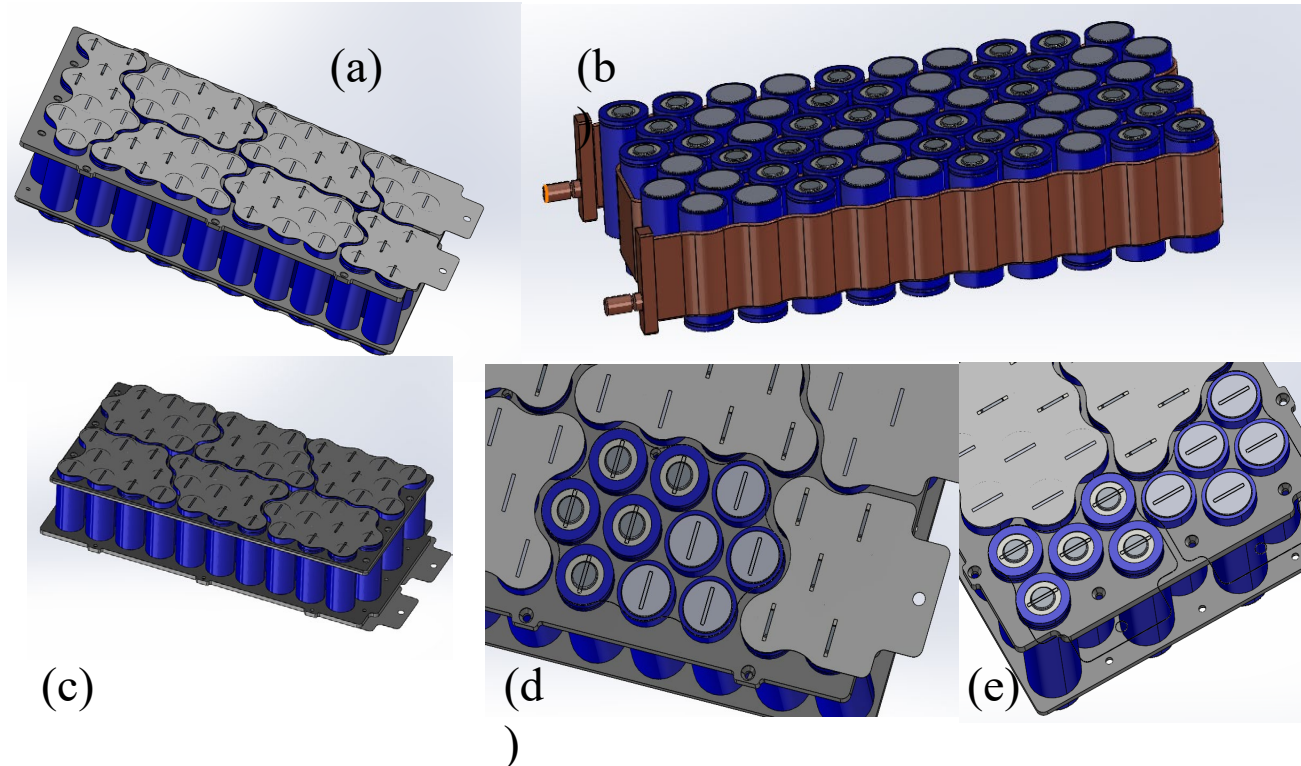
## ➤ Objective

**Study of a battery pack side cooling system for an e-bus.**

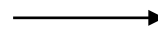
## ➤ Methodology

- **Calculation of heat generated by a battery cell / module:**
  - Calculate parameters for cell model (equivalent conductivities)
  - Apply model to calculate heat generation for different charge/discharge rates (C-rates) of the module
- **Set-up of CFD-CHT model for one cell with side cooling**
- **Flow characterization of side cooling plate:**
  - CFD to determine pressure drop in function of mass flow rate, validation
  - Use cell model results as boundary conditions for CFD-CHT calculations of cooling plate efficiency (heat transfer, coolant temperature evolution)
- **CFD-CHT simulations with small representative module to determine cooling efficiency at various operating conditions:**
  - Analyze cells temperature evolution for different C-rates, coolant mass flow rates, ambient temperatures, ...
- **Validation with full module / pack**

- The connections of the module are arranged according to a 12S 5P configuration.



- The group of 5 cells in parallel is connected on the other face to the next group of 5 cells



- **12S 5P** electrical configuration
- **Nickel** connection tabs

- To design the cooling system , the first step is to characterize the heat generated by the module, i.e. by each cell.
- The cells are 32700 Li-ion, whose properties are given in the table.

Characteristic	Value
Nominal Capacity	6 Ah
Nominal Voltage	3.2 V
Maximum Voltage	3.65 V
Minimum Voltage	2 V
Maximum continuous discharging current	33 A (5.5C)
Maximum continuous charging current	36 A (6C)
Maximum discharging temperature	65 °C
Maximum charging temperature	65 °C

Diameter	0.032 m
Length	0.070 m



## ➤ Parameters needed for the cell model

- Thermal conductivity in axial and radial directions calculated with the different materials conductivities and thicknesses of the jelly roll.

$$k_{rad} = \frac{\ln \frac{r_n}{r_1}}{\sum_{i=1}^{n-1} \frac{\ln \frac{r_{i+1}}{r_i}}{k_i}} = 0,2 \frac{W}{mK}$$

$$k_{ax} = \frac{\sum_{i=1}^{n-1} k_i * A_i}{A_{total}} = 32 \frac{W}{mK}$$

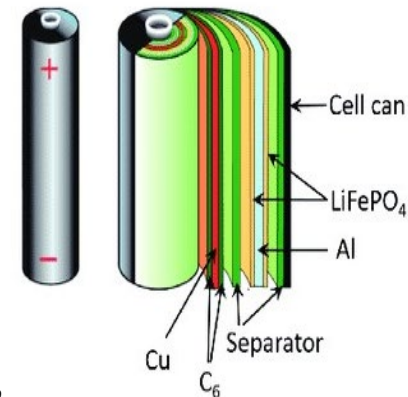
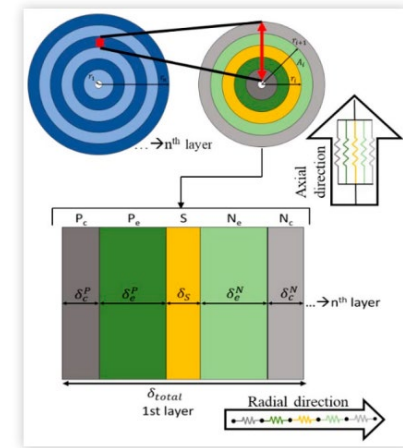
- Positive and negative electrical conductivities

$$\sigma_{eq, positive} = \frac{\sum_{i=1}^{n-1} \sigma_{i,P_c} * A_{i,P_c} + \sum_{i=1}^{n-1} \sigma_{i,P_e} * A_{i,P_e}}{A_{total}(P_c, P_e)}$$

$$\sigma_{eq,p} = 1,62 \cdot 10^6 \text{ S/m}$$

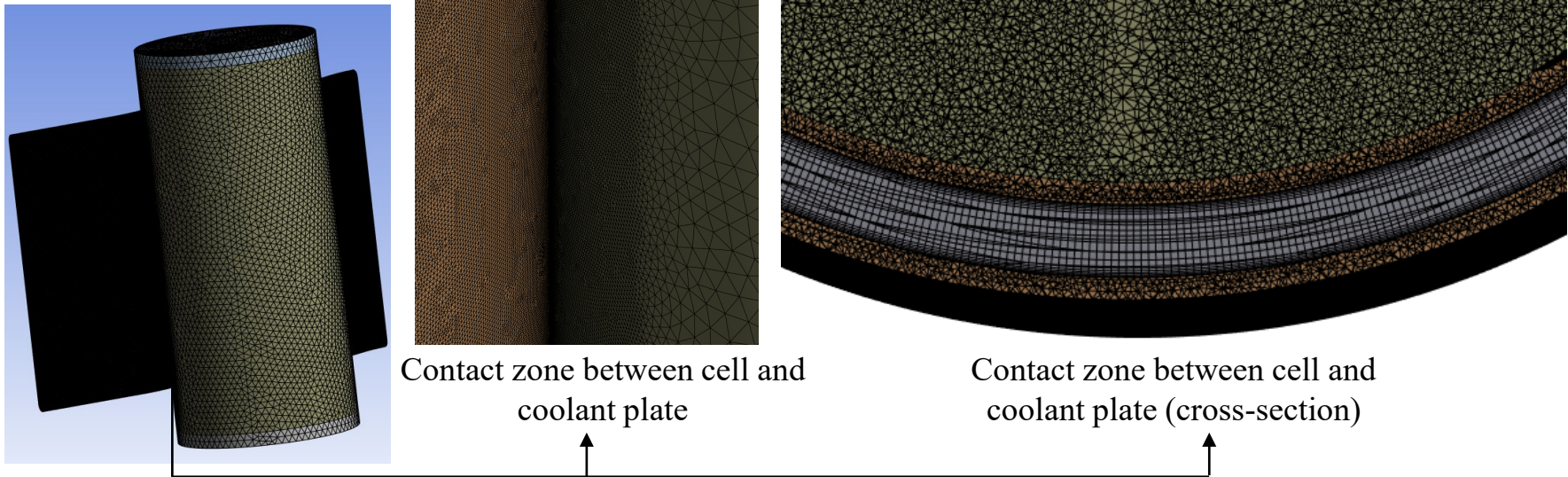
$$\sigma_{eq, negative} = \frac{\sum_{i=1}^{n-1} \sigma_{i,N_c} * A_{i,N_c} + \sum_{i=1}^{n-1} \sigma_{i,N_e} * A_{i,N_e}}{A_{total}(N_c, N_e)}$$

$$\sigma_{eq,n} = 1,49 \cdot 10^6 \text{ S/m}$$





## ➤ One cell model meshing:



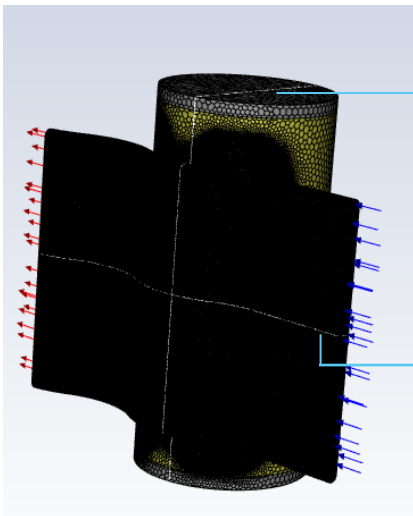
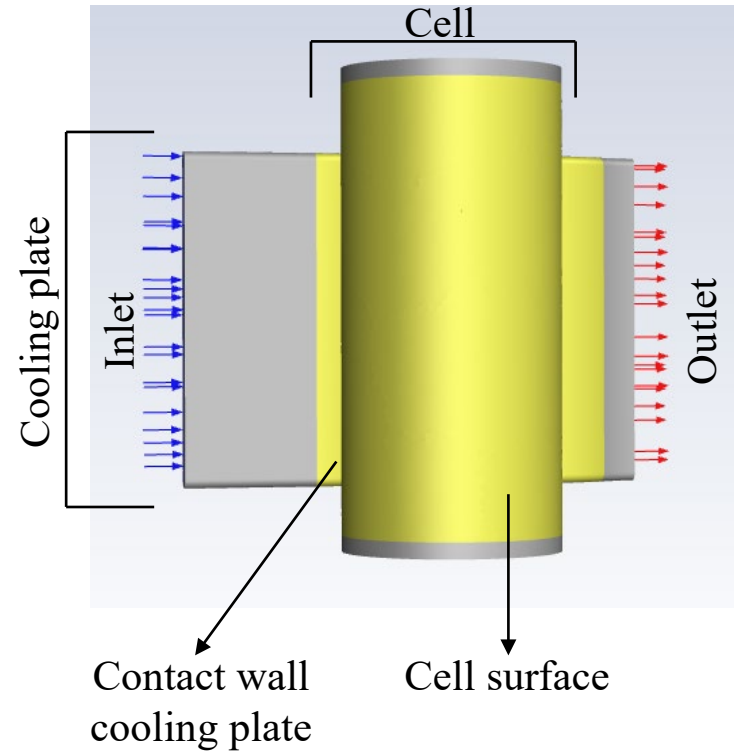
- **Mesh generation:**

- To avoid high number of mesh cells in the contact zones, a *contact mesh sizing* has been separately defined at the contacting surfaces

Number of nodes	5,661,214
Number of elements	23,437,214

## ➤ Boundary conditions:

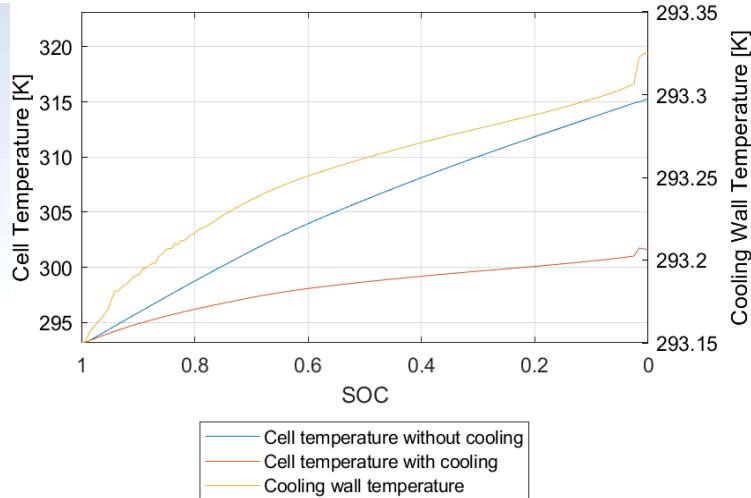
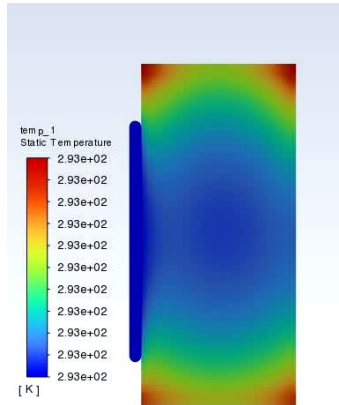
- For cell:
    - 2C discharging condition
    - Ambient temperature: 293.15 K
  - For cooling plate:
    - Inlet mass flow: 7.5 L/min (4.83 m/s)
    - Inlet fluid temperature: 293.15 K
- Fluid was assumed completely stabilised inside the cooling plate.



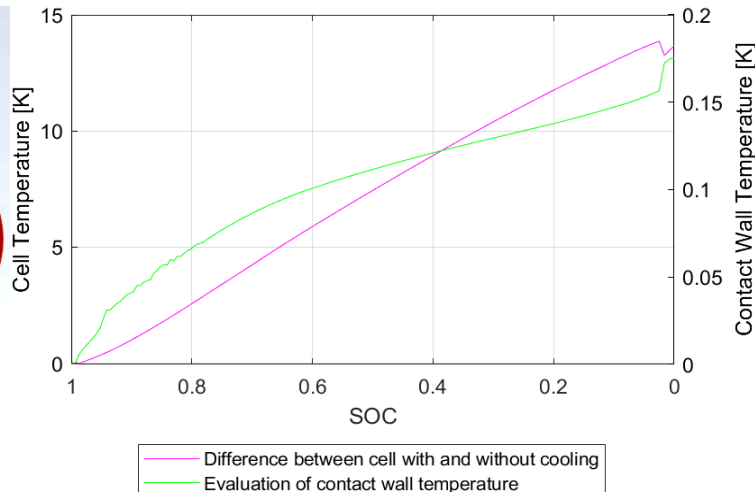
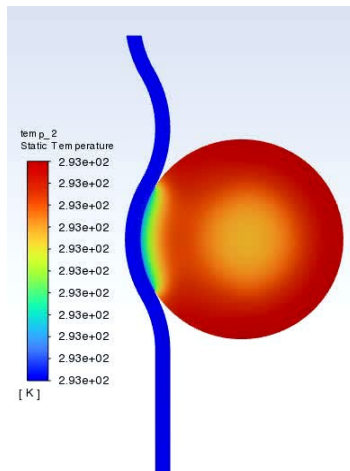
- The white line in the image represents two planes, which were created to observe the temperature distribution between cell and the cooling plate
  - One in vertical direction (considering the centre of the cell)
  - Second in horizontal direction (considering the centre of the cooling plate)



## ➤ Results of one cell CFD-CHT model

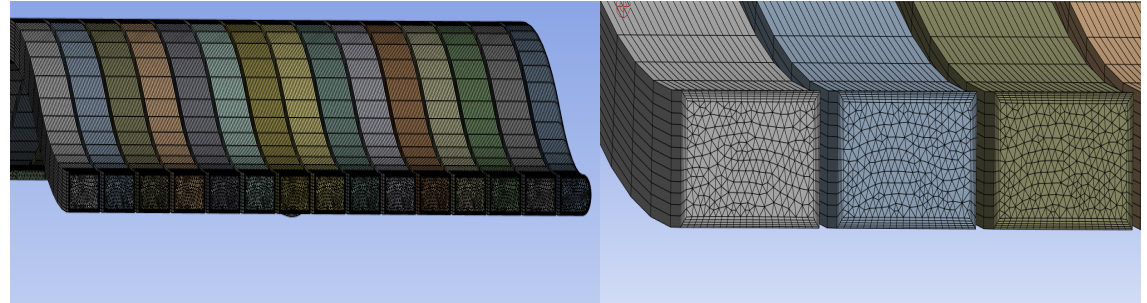
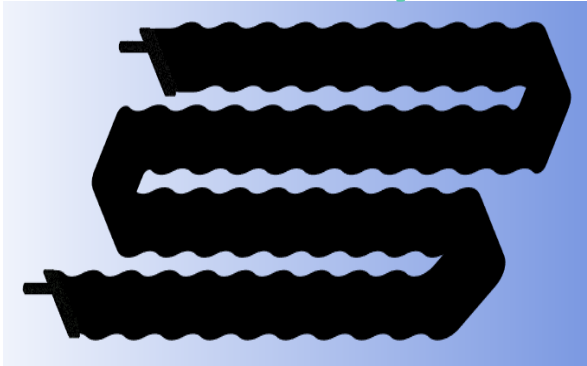


- Cell Temperature at SOC = 0
  - Without cooling plate = 315.32 K
  - With cooling plate = 301.64 K
  - Difference between with and without cooling plate = 13.68 K

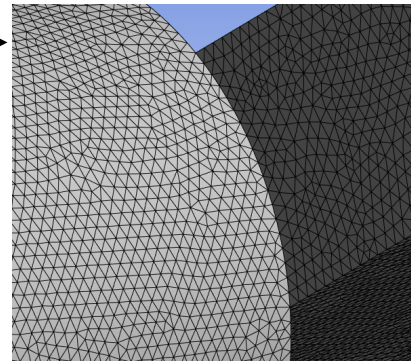
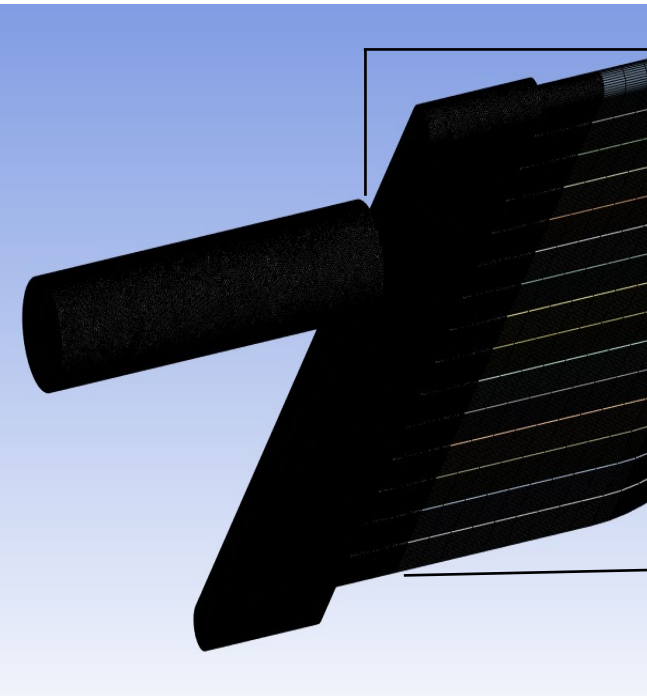


- Coolant contact wall temperature at SOC = 0
  - 293.32 K
  - Total rise in wall temperature from SOC 1 to 0 = 0.17 K

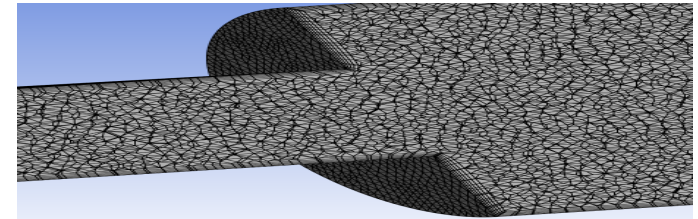
## ➤ Geometry and meshing of cooling plate



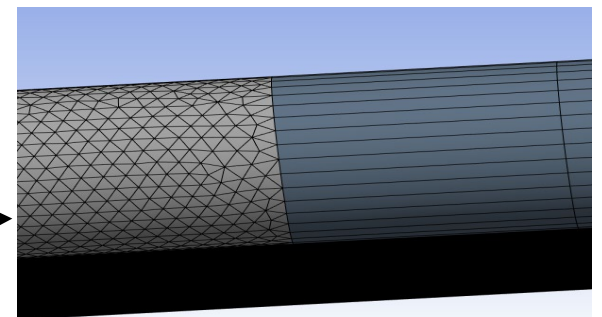
Mesh on and in the channels



Nodes connection and meshing between the circular inlet/outlet and the plenum



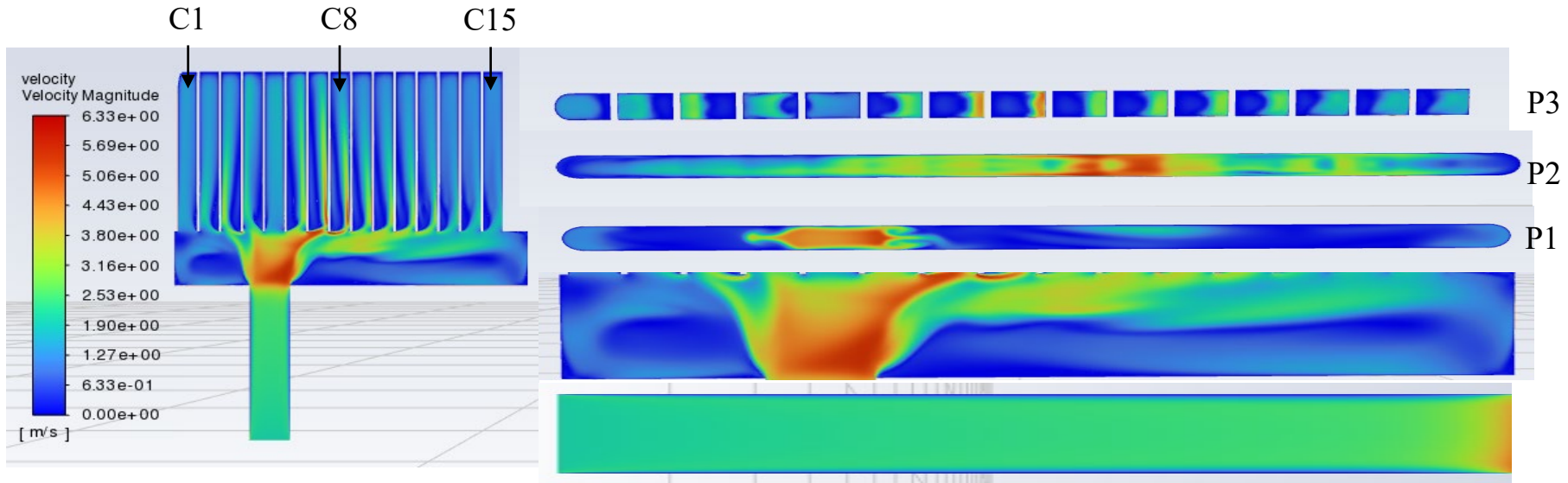
Crosscut-section between the circular inlet/outlet and the plenum



Nodes connection and meshing at the plenum and the channels

Element size: 0.13mm  
Number of nodes: 14082067  
Number of elements: 29626041

## ➤ Boundary conditions and velocity field at inlet



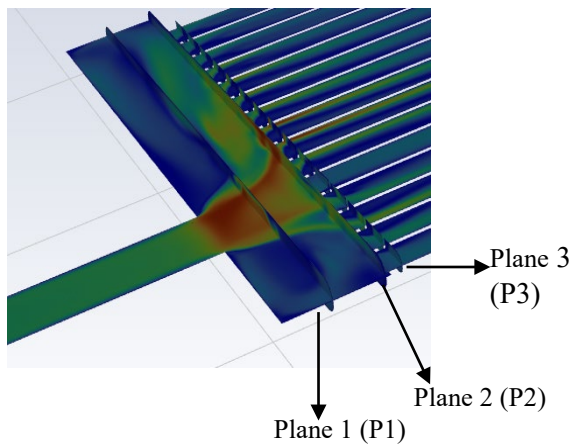
### Boundary conditions:

Inlet mass flow: 3.27 L/min

Fluid inlet temperature: 293.15 °C

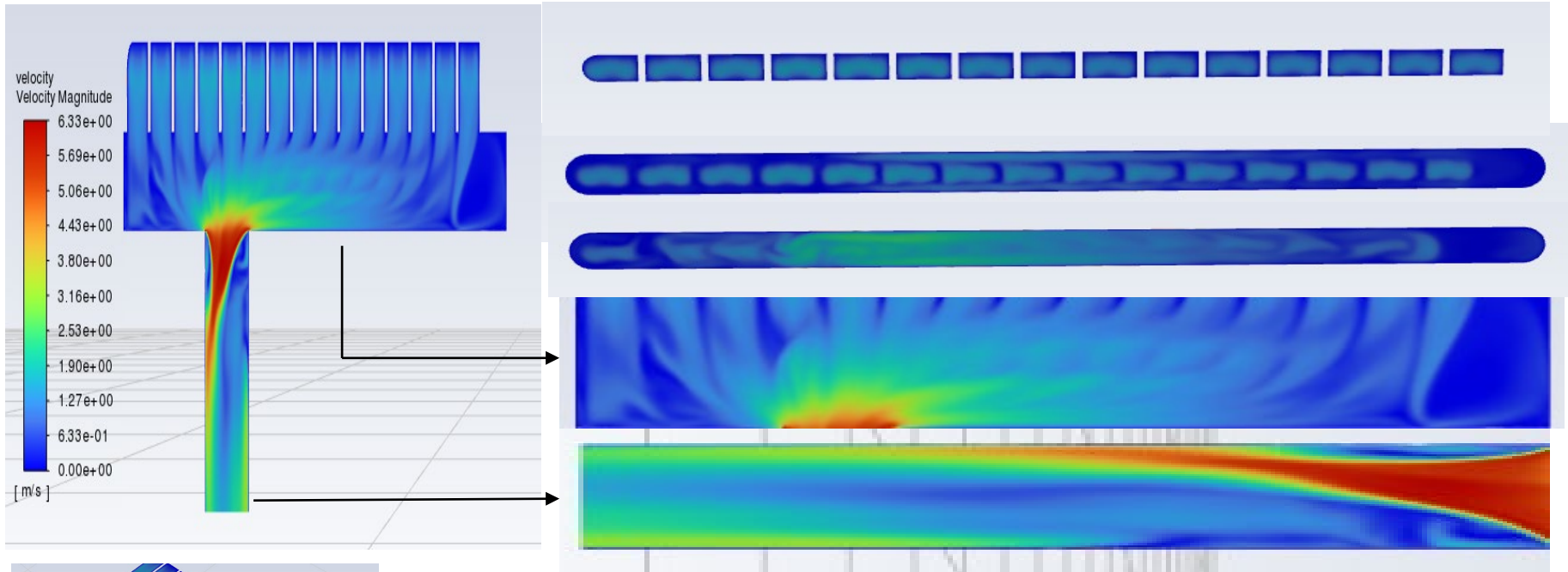
Heat flux on the refrigerant walls: 910 W/m<sup>2</sup>

Coolant: Water Glycol Properties at 20°C	
Density(kg/m <sup>3</sup> )	1082
Viscosity (kg/m s)	0.00487
Specific heat (J/kg K)	3260
Conductivity (W/m K)	0.402





## ➤ Velocity field at outlet

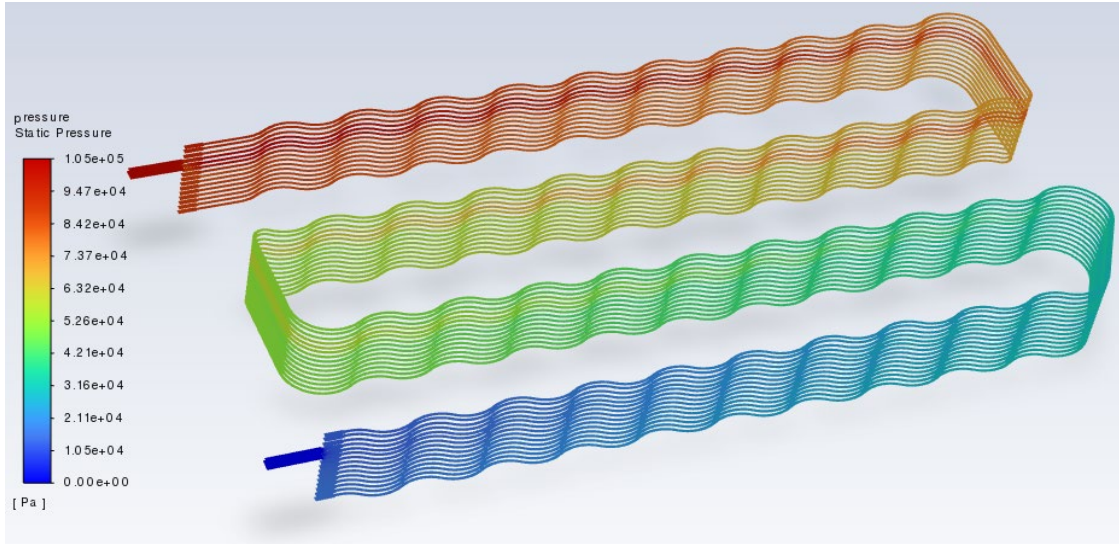


### Results at outlet

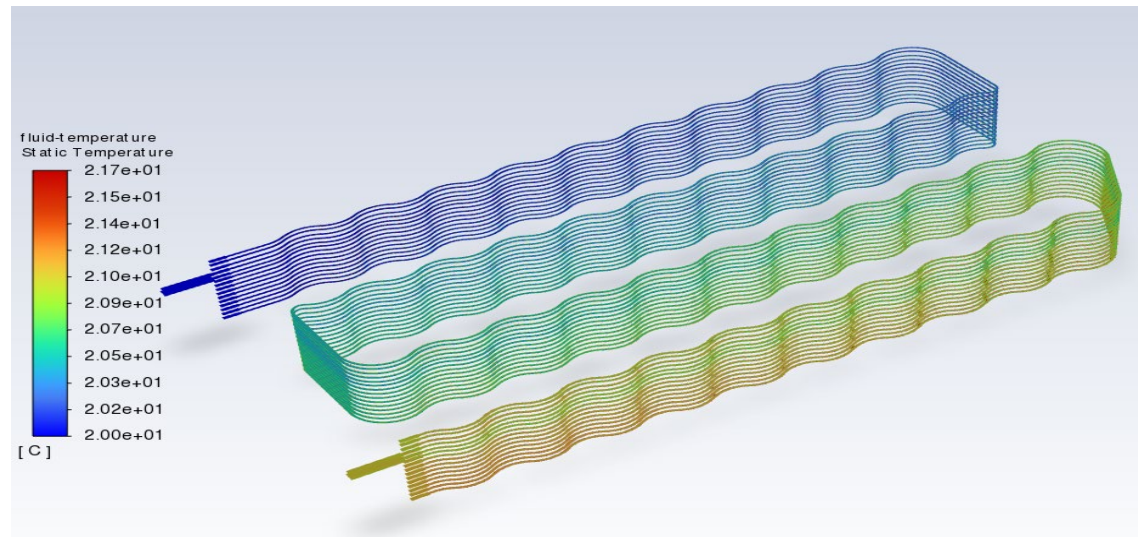
Fluid velocity: 2.11 m/s (3.27 L/min)

- Due to the change in geometry, higher velocity can be seen at the entrance of the outlet
- The velocity stabilises as it moving towards the end of the outlet

## ➤ Pressure field and fluid temperature in cooling plate

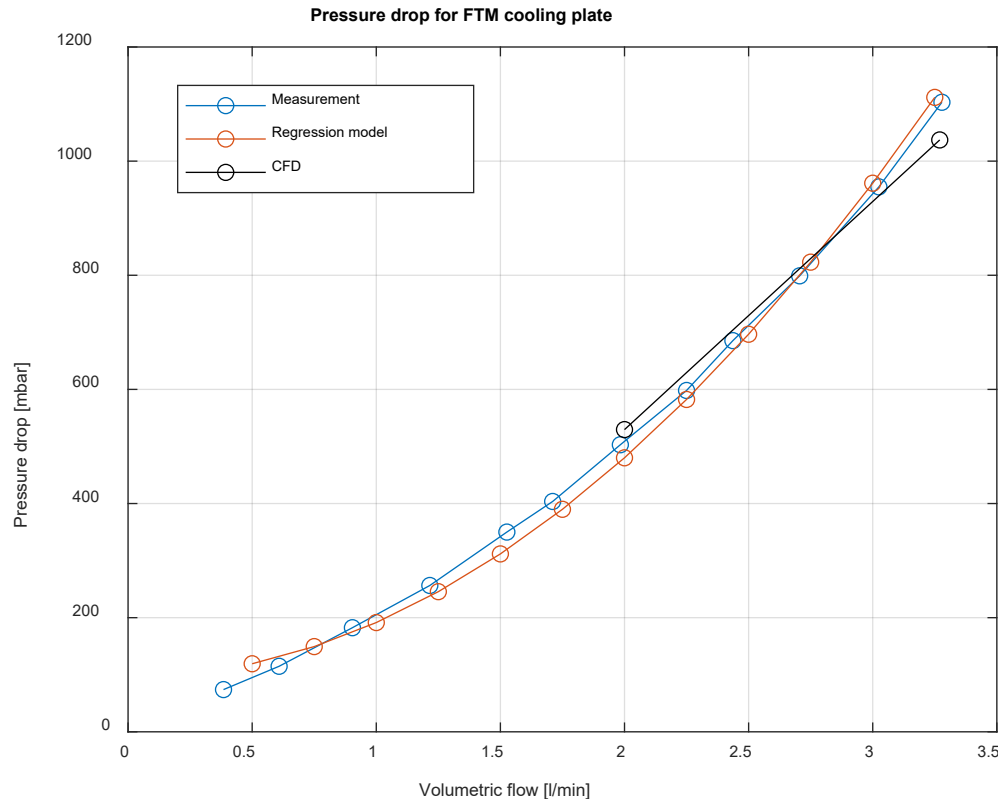


- Pressure gradient difference along channels due to the position of the entry
- The overall pressure drop along the cooling plate **1.03 bar**



- The temperature increase of the coolant between inlet and outlet is **0.88 K**.
- The fluid temperature at the outlet is **294.03 K**.
- Estimated heat transfer coefficient is  **$850.16 \frac{W}{m^2 K}$**

## Validation with experimental measurements



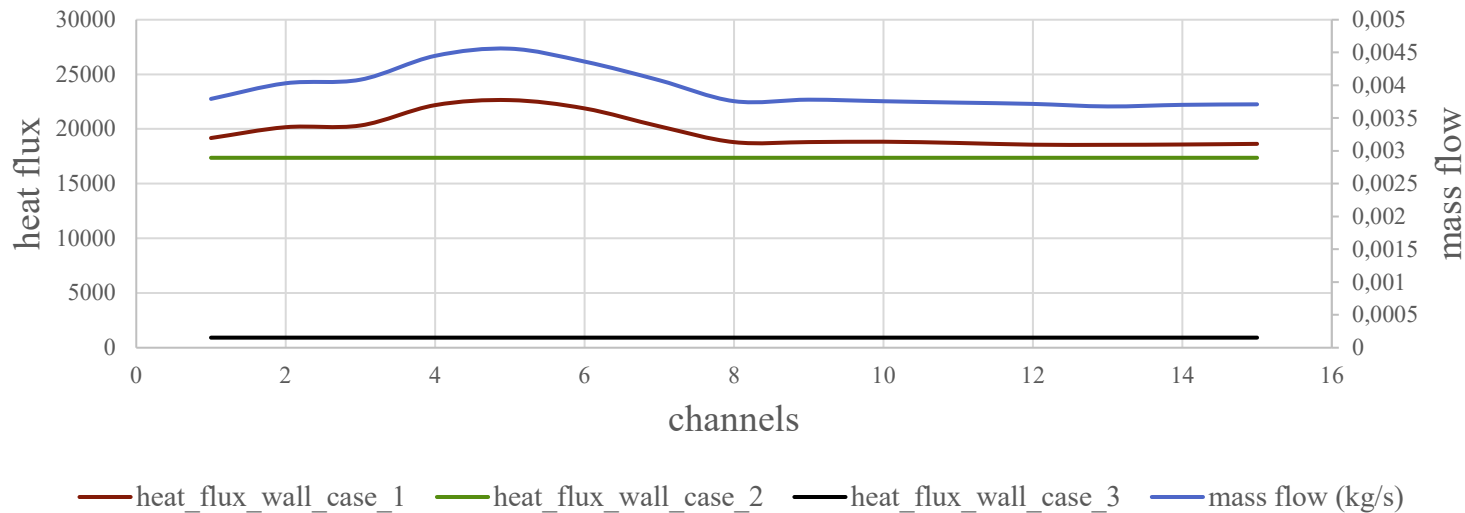
- Good agreement between CFD and experiments.
- Maximum difference found is 6% for 3,27 L/min.
- Differences probably due to micro-channels internal geometry.

Flow rate (L/min)	2	3,27
Temperature at outlet (K)	21,72	20, 88
Pressure loss (bar)	0,53	1,03
Heat transfer coefficient (W/m <sup>2</sup> K)	611,52	850,16



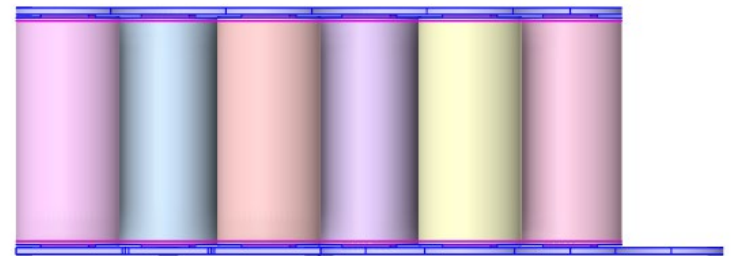
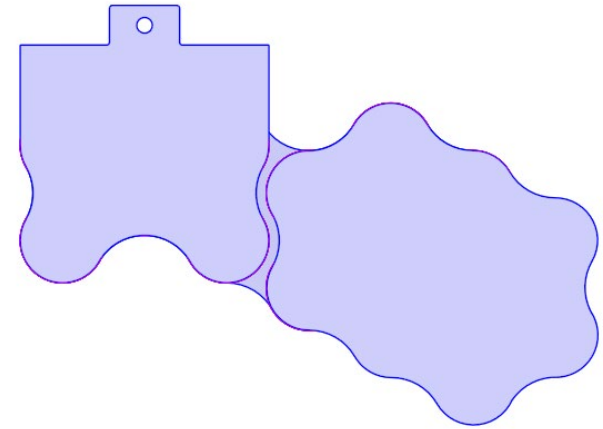
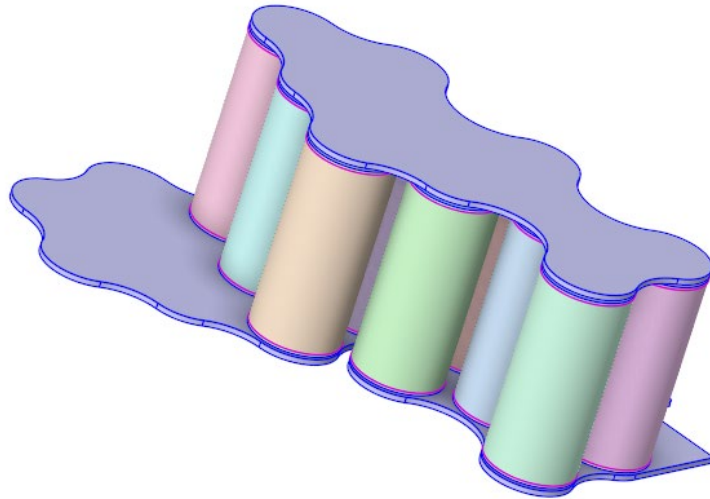
## ➤ Results of heat transfer through cooling plate wall

Cases	Boundary conditions	Fluid outlet temperature (°C)	Heat flux (W/m <sup>2</sup> )	Average heat transfer coefficient (W/(m <sup>2</sup> K))
<b>Case 1 (base case)</b>	Inlet flow rate: 3.27 L/min Fluid inlet temperature: 20 °C Wall temperature: 40°C	39.75	17350	851.53
<b>Case 2</b>	Inlet flow rate: 3.27 L/min Fluid inlet temperature: 20 °C Heat flux: 17350 W/m <sup>2</sup>	39.67	17350	997.09
<b>Case 3</b>	Inlet flow rate: 3.27 L/min Fluid inlet temperature: 20 °C Heat flux: 910 W/m <sup>2</sup>	21.03	910	158.6



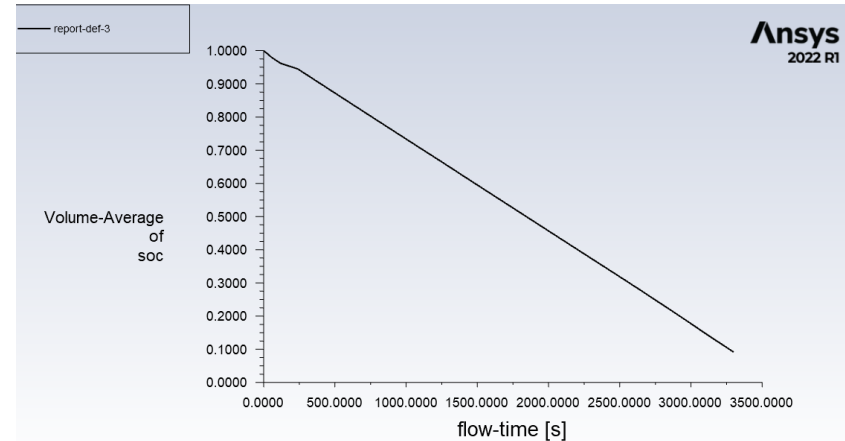
## ➤ Small representative module geometry

- Small 5P2S module representative of the e-bus battery pack module: same cells and connectors, same distribution.

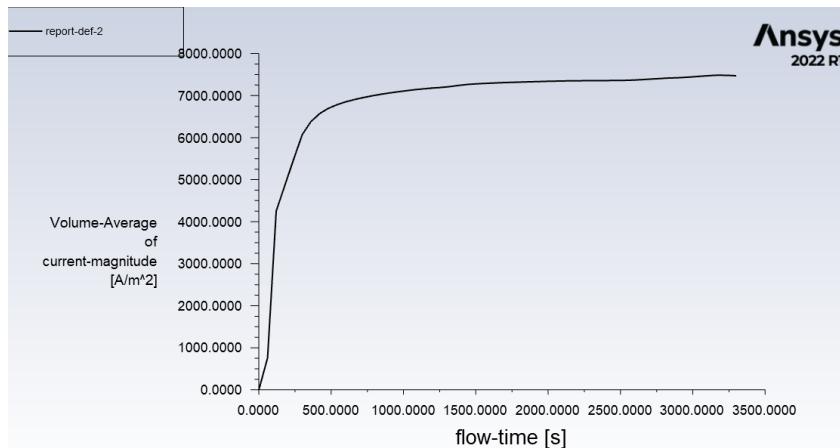


## ➤ Results of CFD-CHT model for small module

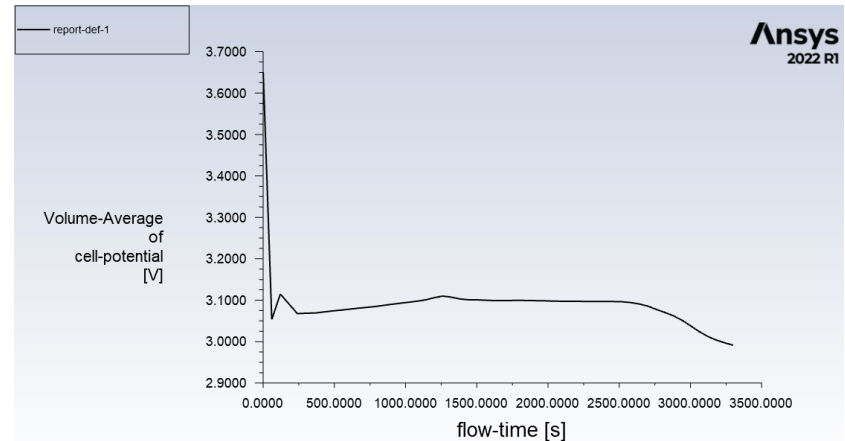
- Voltage max value is set at 3.65V and min at 2V (for SOC 0).
- Current is 6 A for each cell which equals 1C discharge rate.
- 60 hours CPU for one simulation on a Workstation.



SOC evolution during 1C discharge

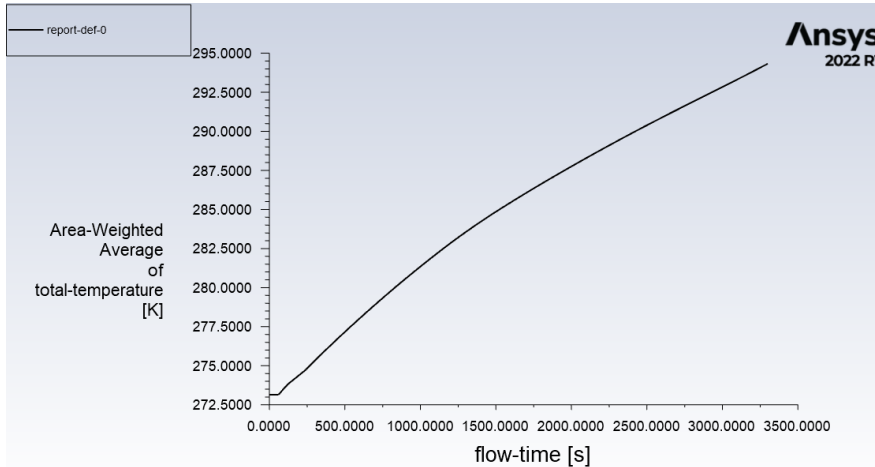


Cell voltage evolution during 1C discharge



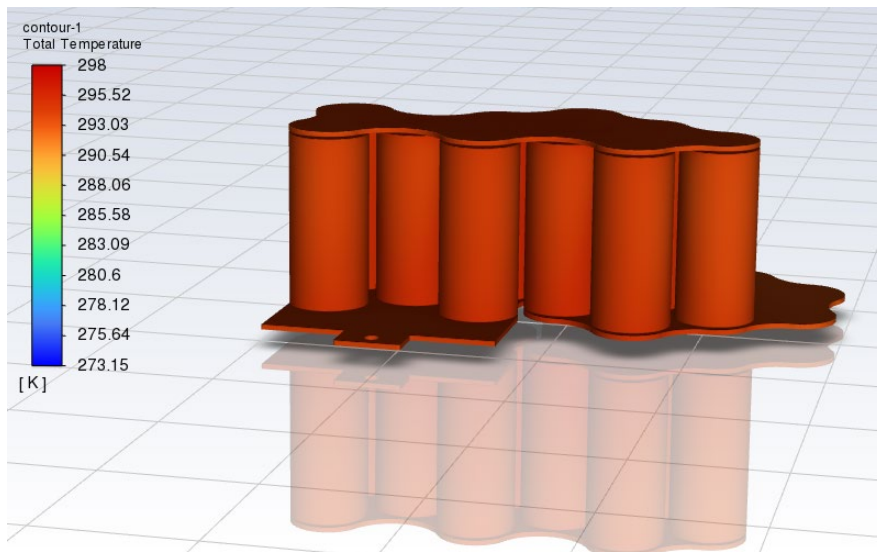
Current voltage evolution during 1C discharge

## ➤ Results of CFD-CHT model for small module



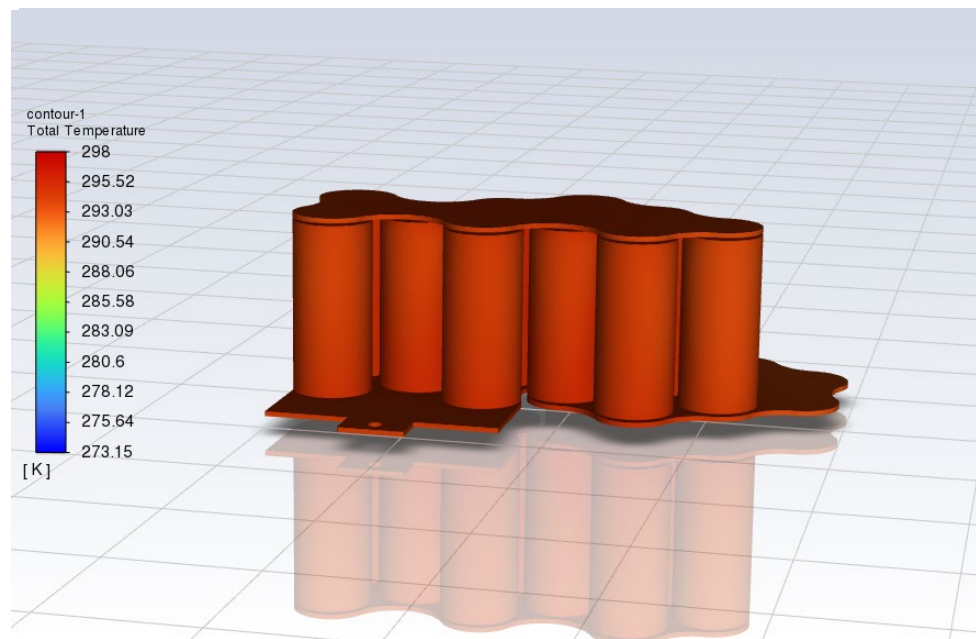
with natural convection

- Temperature increases from 273.15 K to 294.5 K during the 90 percent discharge.



## ➤ Ongoing and future work

- The small module results need more analysis to ensure that the model works properly.
- The full module will then be considered.
- Validation will be possible with experimental measurements of the full module.





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Thank you for your attention

Any questions?